



## INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

<b>(51) International Patent Classification <sup>6</sup> :</b> <b>D21H 23/08 // 21:10, 17:20</b>	<b>A1</b>	<b>(11) International Publication Number:</b> <b>WO 99/55965</b> <b>(43) International Publication Date:</b> 4 November 1999 (04.11.99)
<b>(21) International Application Number:</b> PCT/SE99/00677 <b>(22) International Filing Date:</b> 26 April 1999 (26.04.99)  <b>(30) Priority Data:</b> 98850067.4           27 April 1998 (27.04.98)           EP 60/083,253          27 April 1998 (27.04.98)           US  <b>(71) Applicant (for all designated States except US):</b> AKZO NOBEL N.V. [NL/NL]; P.O. Box 9300, NL-6800 SB Arnhem (NL).  <b>(71) Applicant (for SE only):</b> EKA CHEMICALS AB [SE/SE]; S-445 80 Bohus (SE).  <b>(72) Inventors; and</b> <b>(75) Inventors/Applicants (for US only):</b> KLEMETS, Bore [SE/SE]; Sörkroken 34, S-471 61 Höviksnäs (SE). HÄLLSTRÖM, Hans [SE/SE]; Knut Stangenberg's väg 162, S-131 47 Nacka (SE). ASPLUND, Anna [SE/SE]; Enekullsvägen 40, S-442 50 Ytterby (SE). SIKKAR, Rein [SE/SE]; Vesslestigen 2, S-448 34 Floda (SE).  <b>(74) Agent:</b> NYANDER, Johan; Eka Chemicals AB, Patent Dept., P.O. Box 11556, S-100 61 Stockholm (SE).		<b>(81) Designated States:</b> AL, AM, AT, AU, AZ, BA, BB, BG, BR, BY, CA, CH, CN, CU, CZ, DE, DK, EE, ES, FI, GB, GE, GH, GM, HR, HU, ID, IL, IN, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MD, MG, MK, MN, MW, MX, NO, NZ, PL, PT, RO, RU, SD, SE, SG, SI, SK, SL, TJ, TM, TR, TT, UA, UG, US, UZ, VN, YU, ZA, ZW, ARIPO patent (GH, GM, KE, LS, MW, SD, SL, SZ, UG, ZW), Eurasian patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European patent (AT, BE, CH, CY, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE), OAPI patent (BF, BJ, CF, CG, CI, CM, GA, GN, GW, ML, MR, NE, SN, TD, TG).  <b>Published</b> <i>With international search report.</i>
<b>(54) Title:</b> A PROCESS FOR THE PRODUCTION OF PAPER  <b>(57) Abstract</b> <p>The invention relates to a process for the production of paper from a suspension containing cellulosic fibres, and optional fillers, which comprises adding to the suspension a drainage and retention aid comprising a cationic organic polymer, forming and dewatering the suspension on a wire, wherein the cationic organic polymer has an aromatic group and the suspension which is dewatered on the wire has a conductivity of at least 2.0 mS/cm. The invention further relates to a process for the production of paper from a suspension containing cellulosic fibres, and optional fillers, comprising adding to the suspension a drainage and retention aid comprising a cationic organic polymer having an aromatic group, forming and dewatering the suspension on a wire to obtain a wet web of paper and white water, recirculating the white water and optionally introducing fresh water to form a suspension containing cellulosic fibres, and optional fillers, to be dewatered, wherein the amount of fresh water introduced is less than 30 tons per ton of dry paper produced.</p>		

**FOR THE PURPOSES OF INFORMATION ONLY**

Codes used to identify States party to the PCT on the front pages of pamphlets publishing international applications under the PCT.

AL	Albania	ES	Spain	LS	Lesotho	SI	Slovenia
AM	Armenia	FI	Finland	LT	Lithuania	SK	Slovakia
AT	Austria	FR	France	LU	Luxembourg	SN	Senegal
AU	Australia	GA	Gabon	LV	Latvia	SZ	Swaziland
AZ	Azerbaijan	GB	United Kingdom	MC	Monaco	TD	Chad
BA	Bosnia and Herzegovina	GE	Georgia	MD	Republic of Moldova	TG	Togo
BB	Barbados	GH	Ghana	MG	Madagascar	TJ	Tajikistan
BE	Belgium	GN	Guinea	MK	The former Yugoslav Republic of Macedonia	TM	Turkmenistan
BF	Burkina Faso	GR	Greece			TR	Turkey
BG	Bulgaria	HU	Hungary	ML	Mali	TT	Trinidad and Tobago
BJ	Benin	IE	Ireland	MN	Mongolia	UA	Ukraine
BR	Brazil	IL	Israel	MR	Mauritania	UG	Uganda
BY	Belarus	IS	Iceland	MW	Malawi	US	United States of America
CA	Canada	IT	Italy	MX	Mexico	UZ	Uzbekistan
CF	Central African Republic	JP	Japan	NE	Niger	VN	Viet Nam
CG	Congo	KE	Kenya	NL	Netherlands	YU	Yugoslavia
CH	Switzerland	KG	Kyrgyzstan	NO	Norway	ZW	Zimbabwe
CI	Côte d'Ivoire	KP	Democratic People's Republic of Korea	NZ	New Zealand		
CM	Cameroon			PL	Poland		
CN	China	KR	Republic of Korea	PT	Portugal		
CU	Cuba	KZ	Kazakstan	RO	Romania		
CZ	Czech Republic	LC	Saint Lucia	RU	Russian Federation		
DE	Germany	LI	Liechtenstein	SD	Sudan		
DK	Denmark	LK	Sri Lanka	SE	Sweden		
EE	Estonia	LR	Liberia	SG	Singapore		

A process for the production of paper

This invention relates to papermaking and more specifically to a process for the production of paper in which a cationic organic polymer having an aromatic group is added to a papermaking stock. The process provides improved drainage and retention.

5

Background

In the papermaking art, an aqueous suspension containing cellulosic fibres, and optional fillers and additives, referred to as stock, is fed into a headbox which ejects the stock onto a forming wire. Water is drained from the stock through the forming wire so that a wet web of paper is formed on the wire, and the web is further dewatered and dried in the drying section of the paper machine. Water obtained by dewatering the stock, referred to as white water, which usually contains fine particles, e.g. fine fibres, fillers and additives, is normally recirculated in the papermaking process. Drainage and retention aids are conventionally introduced into the stock in order to facilitate drainage and increase adsorption of fine particles onto the cellulosic fibres so that they are retained with the fibres on the wire. Cationic organic polymers like cationic starch and cationic acrylamide-based polymers are widely used as drainage and retention aids. These polymers can be used alone but more frequently they are used in combination with other polymers and/or with anionic microparticulate materials such as, for example, anionic inorganic particles like colloidal silica, colloidal aluminium-modified silica and bentonite.

20 U.S. Patent Nos. 4,980,025; 5,368,833; 5,603,805; 5,607,552; and 5,858,174; as well as International Patent Application WO 97/18351 disclose the use of cationic and amphoteric acrylamide-based polymers and anionic inorganic particles as stock additives in papermaking. These additives are among the most efficient drainage and retention aids now in use. Similar systems are disclosed in European Patent Application No. 805,234.

25 It has, however, been observed that the performance of drainage and retention aids comprising cationic organic polymers deteriorates when used in stocks with high levels of salt, i.e. high conductivity, and dissolved and colloidal substances. Higher dosages of cationic polymer are normally required in such stocks but usually the drainage and retention effect obtained is still not entirely satisfactory. These problems are noticeable in paper mills where white water is extensively recirculated with the introduction of only low amounts of fresh water into the process, thereby further increasing the accumulation of salts and colloidal materials in the white water and the stock to be dewatered.

30

The Invention

According to the present invention it has been found that improved drainage and retention can be obtained in stocks containing high levels of salt (high conductivity) and colloidal materials and/or in papermaking processes with a high degree of white water

35

closure when using a drainage and retention aid comprising a cationic organic polymer having an aromatic group. More specifically, the present invention relates to a process for the production of paper from a suspension containing cellulosic fibres, and optional fillers, which comprises adding to the suspension a drainage and retention aid comprising

5 a cationic organic polymer, forming and dewatering the suspension on a wire, the process being characterised in that the cationic organic polymer has an aromatic group and the suspension being dewatered on the wire has a conductivity of at least 2.0 mS/cm. The present invention also relates to a process as described in the pre-characterising clause above, the process being further characterised in that it comprises

10 forming and dewatering the suspension on a wire to obtain a wet web containing cellulosic fibres, or paper, and white water, recirculating the white water and optionally introducing fresh water to form a suspension containing cellulosic fibres, and optional fillers, to be dewatered to form paper, wherein the cationic organic polymer has an aromatic group and the amount of fresh water introduced is less than 30 tons per ton of dry paper produced.

15 The invention thus relates to a process as further defined in the claims.

The present invention results in improved drainage and/or retention when using stocks having high contents of salt, and thus having high conductivity levels, and colloidal materials. The present invention also results in improved drainage and/or retention when applied to papermaking processes with extensive white water recirculation and limited

20 fresh water supply and/or processes using fresh water having high salt contents, in particular salts of di- and multivalent cations like calcium. Hereby the present invention makes it possible to increase the speed of the paper machine and to use lower dosages of additives to give a corresponding drainage and/or retention effect, thereby leading to an improved papermaking process and economic benefits.

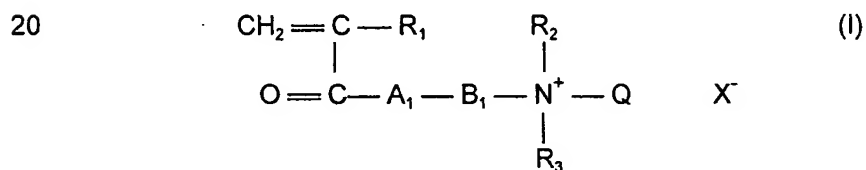
25 The cationic organic polymer having an aromatic group according to this invention, herein also referred to as "main polymer", is capable of functioning as a drainage and retention aid (agent). The term "drainage and retention aid", as used herein, refers to one or more components (aids, agents, or additives) which, when being added to a stock, give better drainage and/or retention than is obtained when not adding

30 the said one or more components. Accordingly, the main polymer provides improved drainage and/or retention, either when used alone or when used in conjunction with one or more additional stock additives. The main polymer can be linear, branched or cross-linked, e.g. in the form of a microparticulate material. Preferably the main polymer is water-soluble or water-dispersable. The aromatic group of the main polymer can be present in the

35 polymer backbone or, preferably, it can be a pendent group attached to or extending from the polymer backbone or be present in a pendent group that is attached to or extending

from the polymer backbone (main chain). Suitable aromatic (aryl) groups include those comprising a phenyl group, optionally substituted, a phenylene group, optionally substituted, and a naphthyl group, optionally substituted, for example groups having the general formulae  $-\text{C}_6\text{H}_5$ ,  $-\text{C}_6\text{H}_4-$ ,  $-\text{C}_6\text{H}_3-$ , and  $-\text{C}_6\text{H}_2-$ , e.g. in the form of phenylene  
 5  $(-\text{C}_6\text{H}_4-)$ , xylylene  $(-\text{CH}_2-\text{C}_6\text{H}_4-\text{CH}_2-)$ , phenyl  $(-\text{C}_6\text{H}_5)$ , benzyl  $(-\text{CH}_2-\text{C}_6\text{H}_5)$ , phenethyl  $(-\text{CH}_2\text{CH}_2-\text{C}_6\text{H}_5)$ , and substituted phenyl (for example  $-\text{C}_6\text{H}_4-\text{Y}$ ,  $-\text{C}_6\text{H}_3\text{Y}_2$ , and  $-\text{C}_6\text{H}_2\text{Y}_3$ ) where one or more substituents (Y) attached to the phenyl ring can be selected from hydroxyl, halides, e.g. chloride, nitro, and hydrocarbon groups having from 1 to 4 carbon atoms.

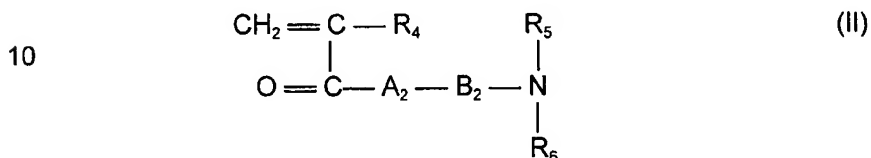
10 The main polymer can be selected from homopolymers and copolymers prepared from one or more monomers comprising at least one monomer having an aromatic group, suitably an ethylenically unsaturated monomer, and the main polymer is suitably a vinyl addition polymer. The term "vinyl addition polymer", as used herein, refers to a polymer prepared by addition polymerization of one or more vinyl monomers or ethylenically  
 15 unsaturated monomers which include, for example, acrylamide-based and acrylate-based monomers. Suitable main polymers include cationic vinyl addition polymers obtained by polymerizing a cationic monomer or a monomer mixture comprising a cationic monomer represented by the general formula (I):



wherein  $\text{R}_1$  is H or  $\text{CH}_3$ ;  $\text{R}_2$  and  $\text{R}_3$  are each or, preferably, an alkyl group having from 1 to 3 carbon atoms, usually 1 to 2 carbon atoms;  $\text{A}_1$  is O or NH;  $\text{B}_1$  is an alkylene group having from 2 to 8 carbon atoms, suitably from 2 to 4 carbon atoms, or a hydroxy propylene group; Q is a substituent containing an aromatic group, suitably a phenyl or substituted phenyl  
 30 group, which can be attached to the nitrogen by means of an alkylene group usually having from 1 to 3 carbon atoms, suitably 1 to 2 carbon atoms, and preferably Q is a benzyl group  $(-\text{CH}_2-\text{C}_6\text{H}_5)$ ; and  $\text{X}^-$  is an anionic counterion, usually a halide like chloride. Examples of suitable monomers represented by the general formula (I) include quaternary monomers obtained by treating dialkylaminoalkyl (meth)acrylates, e.g. dimethylaminoethyl (meth)-  
 35 acrylate, diethylaminoethyl (meth)acrylate and dimethylaminohydroxypropyl (meth)acrylate, and dialkylaminoalkyl (meth)acrylamides, e.g. dimethylaminoethyl (meth)acrylamide, diethylaminoethyl (meth)acrylamide, dimethylaminopropyl (meth)acrylamide, and diethylaminopropyl (meth)acrylamide, with benzyl chloride. Preferred cationic monomers of the

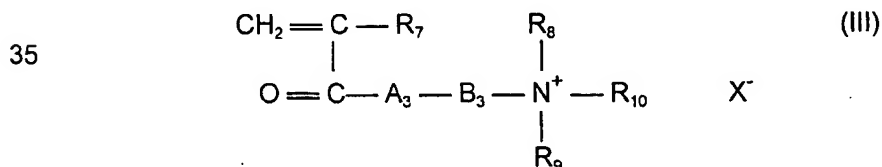
general formula (I) include dimethylaminoethylacrylate benzyl chloride quaternary salt and dimethylaminoethylmethacrylate benzyl chloride quaternary salt.

The main polymer can be a homopolymer prepared from a cationic monomer having an aromatic group or a copolymer prepared from a monomer mixture comprising a cationic monomer having an aromatic group and one or more copolymerizable monomers. Suitable copolymerizable non-ionic monomers include monomers represented by the general formula (II):



wherein  $\text{R}_4$  is H or  $\text{CH}_3$ ;  $\text{R}_5$  and  $\text{R}_6$  are each H or a hydrocarbon group, suitably alkyl, having from 1 to 6, suitably from 1 to 4 and usually from 1 to 2 carbon atoms;  $\text{A}_2$  is O or NH;  $\text{B}_2$  is an alkylene group of from 2 to 8 carbon atoms, suitably from 2 to 4 carbon atoms, or a hydroxy propylene group or, alternatively, A and B are both nothing whereby there is a single bond between C and N ( $\text{O}=\text{C}-\text{NR}_5\text{R}_6$ ). Examples of suitable copolymerizable monomers of this type include (meth)acrylamide; acrylamide-based monomers like N-alkyl (meth)acrylamides and N,N-dialkyl (meth)acrylamides, e.g. N-n-propylacrylamide, N-isopropyl (meth)acrylamide, N-n-butyl (meth)acrylamide, N-isobutyl (meth)acrylamide and N-t-butyl (meth)acrylamide; and dialkylaminoalkyl (meth)acrylamides, e.g. dimethylaminoethyl (meth)acrylamide, diethylaminoethyl (meth)acrylamide, dimethylaminopropyl (meth)acrylamide and diethylaminopropyl (meth)acrylamide; acrylate-based monomers like dialkylaminoalkyl (meth)acrylates, e.g. dimethylaminoethyl (meth)acrylate, diethylaminoethyl (meth)acrylate, t-butylaminoethyl (meth)acrylate and dimethylaminohydroxypropyl acrylate; and vinylamides, e.g. N-vinylformamide and N-vinylacetamide. Preferred copolymerizable non-ionic monomers include acrylamide and methacrylamide, i.e. (meth)acrylamide, and the main polymer is preferably an acrylamide-based polymer.

Suitable copolymerizable cationic monomers include the monomers represented by the general formula (III):



wherein  $\text{R}_7$  is H or  $\text{CH}_3$ ;  $\text{R}_8$ ,  $\text{R}_9$  and  $\text{R}_{10}$  are each H or, preferably, a hydrocarbon group, suitably alkyl, having from 1 to 3 carbon atoms, usually 1 to 2 carbon atoms;  $\text{A}_3$  is O or NH;

B<sub>3</sub> is an alkylene group of from 2 to 4 carbon atoms, suitably from 2 to 4 carbon atoms, or a hydroxy propylene group, and X<sup>-</sup> is an anionic counterion, usually methylsulphate or a halide like chloride. Examples of suitable cationic copolymerizable monomers include acid addition salts and quaternary ammonium salts of the dialkylaminoalkyl (meth)acrylates and dialkylaminoalkyl (meth)acrylamides mentioned above, usually prepared using acids like HCl, H<sub>2</sub>SO<sub>4</sub>, etc., or quaternizing agents like methyl chloride, dimethyl sulphate, etc.; and diallyldimethylammonium chloride. Preferred copolymerizable cationic monomers include dimethylaminoethyl (meth)acrylate methyl chloride quaternary salt and diallyldimethylammonium chloride. Copolymerizable anionic monomers like acrylic acid, methacrylic acid, various sulfonated vinyl addition monomers, etc. can also be employed and, preferably, in minor amounts.

The main polymer according to this invention can be prepared from a monomer mixture generally comprising from 1 to 99 mole%, suitably from 2 to 50 mole% and preferably from 5 to 20 mole% of cationic monomer having an aromatic group, preferably represented by the general formula (I), and from 99 to 1 mole%, suitably from 98 to 50 mole%, and preferably from 95 to 80 mole% of other copolymerizable monomers which preferably comprises acrylamide or methacrylamide ((meth)acrylamide), the monomer mixture suitably comprising from 98 to 50 mole% and preferably from 95 to 80 mole% of (meth)acrylamide, the sum of percentages being 100.

The main polymer can also be selected from polymers prepared by condensation reaction of one or more monomers containing an aromatic group. Examples of such monomers include toluene diisocyanates, bisphenol A, phthalic acid, phthalic anhydride, etc., which can be used in the preparation of cationic polyurethanes, cationic polyamide-amines, etc.

Alternatively, or additionally, the main polymer can be a polymer subjected to aromatic modification using an agent containing an aromatic group. Suitable modifying agents of this type include benzyl chloride, benzyl bromide, N-(3-chloro-2-hydroxypropyl)-N-benzyl-N,N-dimethylammonium chloride, and N-(3-chloro-2-hydroxypropyl) pyridinium chloride. Suitable polymers for such an aromatic modification include vinyl addition polymers. If the polymer contains a tertiary nitrogen which can be quaternized by the modifying agent, the use of such agents usually results in that the polymer is rendered cationic. Alternatively, the polymer to be subjected to aromatic modification can be cationic, for example a cationic vinyl addition polymer.

Usually the charge density of the main polymer is within the range of from 0.1 to 6.0 meqv/g of dry polymer, suitably from 0.2 to 4.0 and preferably from 0.5 to 3.0.

The weight average molecular weight of synthetic main polymers is usually at least about 500,000, suitably above about 1,000,000 and preferably above about 2,000,000. The upper limit is not critical; it can be about 50,000,000, usually 30,000,000 and suitably 25,000,000.

The main polymer of this invention may be in any state of aggregation such as, for example, in solid form, e.g. powders, in liquid form, e.g. solutions, emulsions, dispersions, including salt dispersions, etc. Examples of suitable main polymers for use in this invention include those described in U.S. Patent Nos. 5,169,540; 5,708,071; and European Patent Applications 183,466; 525,751 and 805,234; the disclosures of which are hereby incorporated herein by reference. When being added to the stock, the main polymer is suitably in liquid form, e.g. in the form of an aqueous solution or dispersion.

The main polymer can be added into the stock to be dewatered in amounts which can vary within wide limits depending on, inter alia, type of stock, salt content, type of salts, filler content, type of filler, point of addition, etc. Generally the main polymer is added in an amount that give better retention than is obtained when not adding it. The main polymer is usually added in an amount of at least 0.001%, often at least 0.005% by weight, based on dry stock substance, whereas the upper limit is usually 3% and suitably 1.5% by weight.

In a preferred embodiment of this invention, the main polymer is used in conjunction with an additional stock additive, thereby forming a drainage and retention aid comprising two or more components, usually referred to as drainage and retention aids. The term "drainage and retention aids", as used herein, refers to two or more components (aids, agents or additives) which, when being added to a stock, give better drainage and/or retention than is obtained when not adding the components. Examples of suitable stock additives of this type include anionic microparticulate materials, e.g. anionic organic particles and anionic inorganic particles, water-soluble anionic vinyl addition polymers, low molecular weight cationic organic polymers, aluminium compounds, and combinations thereof. In a preferred aspect of this embodiment, the main polymer is used in conjunction with an anionic microparticulate material, notably with anionic inorganic particles. In another preferred aspect of this embodiment, the main polymer is used in conjunction with anionic inorganic particles and a low molecular weight cationic organic polymer. In yet another preferred aspect of this embodiment, the main polymer is used in conjunction with anionic inorganic particles and an aluminium compound.

Anionic inorganic particles that can be used according to the invention include anionic silica-based particles and clays of the smectite type. It is preferred that the anionic inorganic particles are in the colloidal range of particle size. Anionic silica-based particles, i.e. particles based on  $\text{SiO}_2$  or silicic acid, are preferably used and such particles are usually



supplied in the form of aqueous colloidal dispersions, so-called sols. Examples of suitable silica-based particles include colloidal silica and different types of polysilicic acid. The silica-based sols can also be modified and contain other elements, e.g. aluminium and/or boron, which can be present in the aqueous phase and/or in the silica-based particles. Suitable silica-based particles of this type include colloidal aluminium-modified silica and aluminium silicates. Mixtures of such suitable silica-based particles can also be used. Drainage and retention aids comprising suitable anionic silica-based particles are disclosed in U.S. Patent Nos. 4,388,150; 4,927,498; 4,954,220; 4,961,825; 4,980,025; 5,127,994; 5,176,891; 5,368,833; 5,447,604; 5,470,435; 5,543,014; 5,571,494; 5,573,674; 5,584,966; 5,603,805; 10 5,688,482; and 5,707,493; which are hereby incorporated herein by reference.

Anionic silica-based particles suitably have an average particle size below about 50 nm, preferably below about 20 nm and more preferably in the range of from about 1 to about 10 nm. As conventional in silica chemistry, the particle size refers to the average size of the primary particles, which may be aggregated or non-aggregated. The specific surface area of the silica-based particles is suitably above 50 m<sup>2</sup>/g and preferably above 100 m<sup>2</sup>/g. 15 Generally, the specific surface area can be up to about 1700 m<sup>2</sup>/g and preferably up to 1000 m<sup>2</sup>/g. The specific surface area can be measured by means of titration with NaOH in known manner, e.g. as described by Sears in Analytical Chemistry 28(1956):12, 1981-1983 and in U.S. Patent No. 5,176,891. The given area thus represents the average specific surface area of the particles. 20

In a preferred embodiment of the invention, the anionic inorganic particles are silica-based particles having a specific surface area within the range of from 50 to 1000 m<sup>2</sup>/g, preferably from 100 to 950 m<sup>2</sup>/g. Sols of silica-based particles these types also encompass modified sols like aluminium-containing silica-based sols and boron-containing silica-based sols. Preferably, the silica-based particles are present in a sol having an S-value in the range of from 8 to 45%, preferably from 10 to 30%, containing silica-based particles with a specific surface area in the range of from 300 to 1000 m<sup>2</sup>/g, suitably from 500 to 950 m<sup>2</sup>/g, and preferably from 750 to 950 m<sup>2</sup>/g, which sols can be modified with aluminium and/or boron as mentioned above. For example, the particles can be surface- 25 modified with aluminium to a degree of from 2 to 25% substitution of silicon atoms. The S-value can be measured and calculated as described by Iler & Dalton in J. Phys. Chem. 60(1956), 955-957. The S-value indicates the degree of aggregate or microgel formation and a lower S-value is indicative of a higher degree of aggregation. 30

In yet another preferred embodiment of the invention, the silica-based particles are selected from polysilicic acid and modified polysilicic acid having a high specific surface area, suitably above about 1000 m<sup>2</sup>/g. The specific surface area can be within the range of 35

from 1000 to 1700 m<sup>2</sup>/g and preferably from 1050 to 1600 m<sup>2</sup>/g. The sols of modified polysilicic acid can contain other elements, e.g. aluminium and/or boron, which can be present in the aqueous phase and/or in the silica-based particles. In the art, polysilicic acid is also referred to as polymeric silicic acid, polysilicic acid microgel, polysilicate and polysilicate microgel, which are all encompassed by the term polysilicic acid used herein. Aluminium-containing compounds of this type are commonly also referred to as polyaluminosilicate and polyaluminosilicate microgel, which are both encompassed by the terms colloidal aluminium-modified silica and aluminium silicate used herein.

Clays of the smectite type that can be used in the process of the invention are known in the art and include naturally occurring, synthetic and chemically treated materials. Examples of suitable smectite clays include montmorillonite/bentonite, hectorite, beidelite, nontronite and saponite, preferably bentonite and especially such bentonite which after swelling preferably has a surface area of from 400 to 800 m<sup>2</sup>/g. Suitable clays are disclosed in U.S. Patent Nos. 4,753,710; 5,071,512; and 5,607,552, which are hereby incorporated herein by reference.

Anionic organic particles that can be used according to the invention include highly cross-linked anionic vinyl addition polymers, suitably copolymers comprising an anionic monomer like acrylic acid, methacrylic acid and sulfonated or phosphonated vinyl addition monomers, usually copolymerized with nonionic monomers like (meth)acrylamide, alkyl (meth)acrylates, etc. Useful anionic organic particles also include anionic condensation polymers, e.g. melamine-sulfonic acid sols. Water-soluble anionic vinyl addition polymers that can be used according to the invention include copolymers comprising an anionic monomer like acrylic acid, methacrylic acid and sulfonated vinyl addition monomers, usually copolymerized with nonionic monomers like acrylamide, alkyl acrylates, etc., for example those disclosed in U.S. Patent Nos. 5,098,520 and 5,185,062, the teachings of which are incorporated herein by reference.

Low molecular weight (hereinafter LMW) cationic organic polymers that can be used according to the invention include those commonly referred to and used as anionic trash catchers (ATC). ATC's are known in the art as neutralizing and/or fixing agents for detrimental anionic substances present in the stock and the use thereof in combination with drainage and/or retention aids often provide further improved drainage and/or retention. The LMW cationic organic polymer can be derived from natural or synthetic sources, and preferably it is an LMW synthetic polymer. Suitable organic polymers of this type include LMW highly charged cationic organic polymers such as polyamines, polyamidoamines, polyethyleneimines, homo- and copolymers based on diallyldimethyl ammonium chloride, (meth)acrylamides and (meth)acrylates. In relation to the molecular weight of the main

polymer, the molecular weight of the LMW cationic organic polymer is preferably lower; it is suitably at least 2,000 and preferably at least 10,000. The upper limit of the molecular weight is usually about 700,000, suitably about 500,000 and usually about 200,000.

Aluminium compounds that can be used according to the invention include alum,  
5 aluminates, aluminium chloride, aluminium nitrate and polyaluminium compounds, such as polyaluminium chlorides, polyaluminium sulphates, polyaluminium compounds containing both chloride and sulphate ions, polyaluminium silicate-sulphates, and mixtures thereof. The polyaluminium compounds may also contain other anions than chloride ions, for example anions from sulfuric acid, phosphoric acid, organic acids such as citric acid and  
10 oxalic acid.

Components of drainage and retention aids according to the invention can be added to the stock in conventional manner and in any order. When using drainage and retention aids comprising a main polymer and an anionic microparticulate material, notably anionic inorganic particles, it is preferred to add the main polymer to the stock  
15 before adding the microparticulate material, even if the opposite order of addition may be used. It is further preferred to add the main polymer before a shear stage, which can be selected from pumping, mixing, cleaning, etc., and to add the anionic particles after that shear stage. When using an LMW cationic organic polymer or an aluminium compound, such components are preferably introduced into the stock prior to introducing the main  
20 polymer, optionally used in conjunction with an anionic microparticulate material. Alternatively, the LMW cationic organic polymer and the main polymer can be introduced into stock essentially simultaneously, either separately or in admixture, for example as disclosed in U.S. Patent No. 5,858,174, which is hereby incorporated herein by reference. The LMW cationic organic polymer and the main polymer are preferably introduced into the  
25 stock prior to introducing an anionic microparticulate material.

The drainage and retention aid(s) according to the invention can be added to the stock to be dewatered in amounts which can vary within wide limits depending on, inter alia, type and number of components, type of stock, salt content, type of salts, filler content, type of filler, point of addition, degree of white water closure, etc. Generally the aid(s) are added  
30 in amounts that give better drainage and/or retention than is obtained when not adding the components. The main polymer is usually added in an amount of at least 0.001%, often at least 0.005% by weight, based on dry stock substance, and the upper limit is usually 3% and suitably 1.5% by weight. Similar amounts are suitable for water-soluble anionic vinyl addition polymers, if used. When using an anionic microparticulate material in  
35 the process, the total amount added is usually at least 0.001% by weight, often at least 0.005% by weight, based on dry substance of the stock, and the upper limit is usually 1.0%

and suitably 0.6% by weight. When using anionic silica-based particles, the total amount added is suitably within the range of from 0.005 to 0.5% by weight, calculated as  $\text{SiO}_2$  and based on dry stock substance, preferably within the range of from 0.01 to 0.2% by weight. When using an LMW cationic organic polymer in the process, it can be added in an amount  
5 of at least 0.05%, based on dry substance of the stock to be dewatered. Suitably, the amount is in the range of from 0.07 to 0.5%, preferably in the range from 0.1 to 0.35%. When using an aluminium compound in the process, the total amount introduced into the stock to be dewatered depends on the type of aluminium compound used and on other effects desired from it. It is for instance well known in the art to utilize aluminium  
10 compounds as precipitants for rosin-based sizing agents. The total amount added is usually at least 0.05%, calculated as  $\text{Al}_2\text{O}_3$  and based on dry stock substance. Suitably the amount is in the range of from 0.5 to 3.0%, preferably in the range from 0.1 to 2.0%.

The process of this invention is preferably used in the manufacture of paper from a suspension containing cellulosic fibers, and optional fillers, i.e. a stock, which has a high  
15 conductivity. Usually, the conductivity of the stock that is dewatered on the wire is at least 2.0 mS/cm, suitably at least 3.5 mS/cm, preferably at least 5.0 mS/cm and most preferably at least 7.5 mS/cm. Conductivity can be measured by standard equipment such as, for example, a WTW LF 539 instrument supplied by Christian Berner. The values referred to above are suitably determined by measuring the conductivity of the cellulosic suspension  
20 that is fed into or present in the headbox of the paper machine or, alternatively, by measuring the conductivity of white water obtained by dewatering the suspension. High conductivity levels mean high contents of salts (electrolytes), where the various salts can be based on mono-, di- and multivalent cations like alkali metals, e.g.  $\text{Na}^+$  and  $\text{K}^+$ , alkaline earths, e.g.  $\text{Ca}^{2+}$  and  $\text{Mg}^{2+}$ , aluminium ions, e.g.  $\text{Al}^{3+}$ ,  $\text{Al}(\text{OH})^{2+}$  and polyaluminium ions, and  
25 mono-, di- and multivalent anions like halides, e.g.,  $\text{Cl}^-$ , sulfates, e.g.  $\text{SO}_4^{2-}$  and  $\text{HSO}_4^-$ , carbonates, e.g.  $\text{CO}_3^{2-}$  and  $\text{HCO}_3^-$ , silicates and lower organic acids. The invention is particularly useful in the manufacture of paper from stocks having high contents of salts of di- and multivalent cations, and usually the content of di- and multivalent cations is at least 200 ppm, suitably at least 300 ppm and preferably at least 400 ppm. The salts can be  
30 derived from the stock preparation stage, i.e. from the materials used to form the stock, e.g. water, cellulosic fibres and fillers, in particular in integrated mills where a concentrated aqueous fibre suspension from the pulp mill normally is mixed with water to form a dilute suspension suitable for paper manufacture in the paper mill. The salt may also be derived from various additives introduced into the stock, from the fresh water supplied to the  
35 process, etc. Further, the content of salts is usually higher in processes where white water

is extensively recirculated, which may lead to considerable accumulation of salts in the water circulating in the process.

The present invention further encompasses papermaking processes where white water is extensively recirculated (recycled), i.e. with a high degree of white water closure, for example where from 0 to 30 tons of fresh water are used per ton of dry paper produced, usually less than 20, suitably less than 15, preferably less than 10 and notably less than 5 tons of fresh water per ton of paper. Recirculation of white water obtained in the process suitably comprises mixing the white water with cellulosic fibres and/or optional fillers to form a suspension to be dewatered; preferably it comprises mixing the white water with a suspension containing cellulosic fibres, and optional fillers, before the suspension enters the forming wire for dewatering. The white water can be mixed with the suspension before, between, simultaneous with or after introducing the components of drainage and retention aids, if used; and before, simultaneous with or after introducing the main polymer. Fresh water can be introduced in the process at any stage; for example, it can be mixed with cellulosic fibres in order to form a suspension, and it can be mixed with a suspension containing cellulosic fibres to dilute it so as to form the suspension to be dewatered, before, simultaneous with or after mixing the stock with white water and before, between, simultaneous with or after introducing the components of drainage and retention aids, if used; and before, simultaneous with or after introducing the main polymer.

Further additives which are conventional in papermaking can of course be used in combination with the additive(s) according to the invention, such as, for example, dry strength agents, wet strength agents, optical brightening agents, dyes, sizing agents like rosin-based sizing agents and cellulose-reactive sizing agents, e.g. ketene dimers and succinic anhydrides, etc. The cellulosic suspension, or stock, can also contain mineral fillers of conventional types such as, for example, kaolin, china clay, titanium dioxide, gypsum, talc and natural and synthetic calcium carbonates such as chalk, ground marble and precipitated calcium carbonate.

The process of this invention is used for the production of paper. The term "paper", as used herein, of course include not only paper and the production thereof, but also other cellulosic fibre-containing sheet or web-like products, such as for example board and paperboard, and the production thereof. The process can be used in the production of paper from different types of suspensions of cellulose-containing fibres and the suspensions should suitably contain at least 25% by weight and preferably at least 50% by weight of such fibres, based on dry substance. The suspension can be based on fibres from chemical pulp such as sulphate, sulphite and organosolv pulps, mechanical pulp such as thermomechanical pulp, chemo-thermomechanical pulp, refiner pulp and groundwood

pulp, from both hardwood and softwood, and can also be based on recycled fibres, optionally from de-inked pulps, and mixtures thereof.

The invention is further illustrated in the following Examples which, however, are not intended to limit the same. Parts and % relate to parts by weight and % by weight, respectively, unless otherwise stated.

#### Example 1 (Comparison)

Drainage performance was evaluated by means of a Dynamic Drainage Analyser (DDA), available from Akribi, Sweden, which measures the time for draining a set volume of stock through a wire when removing a plug and applying vacuum to that side of the wire opposite to the side on which the stock is present.

The furnish used was based on 70% by weight of pulp of bleached birch/pine sulphate (60/40) refined to 200°C SF and 30% by weight of ground marble. Stock volume was 800 ml, consistency 0.3% and pH about 8.

Conductivity of the stock was adjusted to 0.47 mS/cm by addition of sodium sulphate. The stock was stirred in a baffled jar at a speed of 1500 rpm throughout the test and chemicals additions were conducted as follows: i) adding cationic polymer to the stock followed by stirring for 30 seconds, ii) adding anionic inorganic particles to the stock followed by stirring for 15 seconds, iii) draining the stock while automatically recording the drainage time.

The polymers used for in the test series were P1) a cationic copolymer prepared by polymerisation of acrylamide (90 mole%) and acryloxyethyltrimethylammonium chloride (10 mole%) and having an average molecular weight of about 6,000,000; and P2) a cationic copolymer prepared by polymerisation of acrylamide (90 mole%) and acryloxyethyltrimethylammonium chloride (10 mole%) and having an average molecular weight of about 6,000,000. The polymers P1 and P2 were dissolved in water and used as 0.1% aqueous solutions.

The anionic inorganic particles used were silica-based particles of the type disclosed in U.S. Patent No. 5,368,833. The sol had an S-value of about 25% and contained silica particles with a specific surface area of about 900 m<sup>2</sup>/g which were surface-modified with aluminium to a degree of 5%. The silica-based particles were added in an amount of 1.0 kg/ton, calculated as SiO<sub>2</sub> and based on dry stock system.

Table 1 shows the drainage time at various dosages of P1 and P2, calculated as dry polymer on dry stock system.

13  
Table 1

Test No.	Polymer Dosage [kg/t]	SiO <sub>2</sub> Dosage [kg/t]	Conductivity [mS/cm]	Dewatering time [s]	
				P1	P2
1	0	0	0.47	18.4	18.4
2	1	1	0.47	12.5	10.6
3	1.5	1	0.47	6.9	5.6
4	2	1	0.47	4.9	4.3

#### Example 2 (Comparison)

Dewatering and retention effect was evaluated by means of the DDA used in Example 1 in combination with a nephelometer. First pass retention was evaluated by measuring the turbidity of the filtrate, the white water, obtained by draining the stock.

The furnish used was based on 56% by weight of peroxide bleached TMP/SGW pulp (80/20), 14% by weight of bleached birch/pine sulphate pulp (60/40) refined to 200° CSF and 30% by weight of china clay. To the stock was added 40 g/l of a colloidal fraction, bleach water from an SC mill, filtrated through a 5 µm screen and concentrated with an UF filter, cut off 200,000. Stock volume was 800 ml, consistency 0.14% and pH was adjusted to 4.0 using dilute sulphuric acid. The conductivity was adjusted by addition of calcium chloride (60 ppm Ca<sup>2+</sup>), magnesium sulphate (18 ppm Mg<sup>2+</sup>) and sodium bicarbonate (134 ppm HCO<sub>3</sub><sup>-</sup>).

The polymers and anionic inorganic particles according to Example 1 were similarly used in this test series. Two dosages of polymers were used, 1 kg/t and 2 kg/t, respectively, calculated as dry polymer on dry stock system. Table 2 shows the dewatering and retention effect at various dosages of silica-based particles, calculated as SiO<sub>2</sub> and based on dry stock system.

Table 2

Test No.	Polymer dosage [kg/t]	SiO <sub>2</sub> Dosage [kg/t]	Conductivity [mS/cm]	Dewatering time [s]		Turbidity [NTU]	
				P1	P2	P1	P2
1	1	0	1.375	21.2	18.7	63	55
2	1	1	1.375	17.2	16.1	67	60
3	1	2	1.375	21.2	18.6	66	57
4	2	0	1.375	15.2	14.2	47	45
5	2	1	1.375	11	9.9	47	47
6	2	2	1.375	11.4	10.8	45	50

**Example 3**

In this test series, the dewatering and retention effect was evaluated according to the procedure described in Example 2.

The furnish used was the same as used in Example 2. Stock volume was 800 ml and pH about 7. The conductivity was adjusted by addition of calcium chloride, thus simulating a very high electrolyte content and a high degree of white water closure.

The polymers and anionic inorganic particles according to Example 1 were similarly used in this test series.

Table 3 shows the dewatering and retention effect at various dosages of silica-based particles, calculated as SiO<sub>2</sub> and based on dry stock system.

**Table 3**

Test No.	Polymer Dosage [kg/t]	SiO <sub>2</sub> Dosage [kg/t]	Conductivity [mS/cm]	Dewatering time [s]		Turbidity [NTU]	
				P1	P2	P1	P2
			990 ppm Ca <sup>2+</sup>				
1	2	0	5.5	14.2	19.2	42	64
2	2	1	5.5	10.8	13.9	41	43
3	2	2	5.5	7.7	9.5	35	36
4	2	3	5.5	7.3	8.9	32	39
			1300 ppm Ca <sup>2+</sup>				
5	2	0	7.0	16.2	23.0	46	50
6	2	1	7.0	10.0	17.1	40	45
7	2	2	7.0	7.5	13.6	36	44
8	2	3	7.0	7.7	11.7	34	44
			1930 ppm Ca <sup>2+</sup>				
9	2	0	10.0	18.7	22.0	44	58
10	2	1	10.0	11.6	23.3	39	52
11	2	2	10.0	8.2	15.8	36	53
12	2	3	10.0	8.0	15.4	41	47

**Example 4**

In this test series, the dewatering effect was evaluated with a "Canadian Standard Freeness Tester" which is the conventional method for characterising drainage according to SCAN-C 21:65. All additions of chemicals were made in a "Britt Dynamic Drainage Jar" with blocked outlet at a stirring speed of 1000 rpm during 45 seconds according to the procedure of Example 1 and the stock system was then transferred to the Freeness apparatus. Here the smallest hole in the bottom of the Freeness tester was blocked and the time for 400 ml of furnish to filtrate through the screen was measured. The stock was taken from a closed mill using waste paper. Consistency was 0.14%,



conductivity 8.0 mS/cm and pH about 7. Table 4 shows the dewatering effect at various dosages of silica-based particles, calculated as SiO<sub>2</sub> and based on dry stock system

Table 4

Test No.	Polymer dosage [kg/t]	SiO <sub>2</sub> Dosage [kg/t]	Conductivity [mS/cm]	Dewatering time [s]	
				P1	P2
1	0.6	0	8.0	100.4	103.2
2	0.6	0.25	8.0	66.4	92.5
3	0.6	0.5	8.0	58.3	85.8
4	0.6	0.75	8.0	50.0	76.0
5	0.6	1	8.0	44.6	79.2

#### 5 Example 5

In this test series, the dewatering effect was evaluated as in Example 3, except that both sodium acetate (550 ppm Na<sup>+</sup>) and calcium chloride (1300 ppm Ca<sup>2+</sup>) was used to adjust the conductivity.

The polymers and anionic inorganic particles according to Example 1 were similarly used in this test series.

Table 5 shows the dewatering effect at various dosages of silica-based particles, calculated as SiO<sub>2</sub> and based on dry stock system.

Table 5

Test No.	Polymer dosage [kg/t]	SiO <sub>2</sub> dosage [kg/t]	Conductivity [mS/cm]	Dewatering time [s]	
				P1	P2
1	2	1	2.5	16.1	18.2
2	1	3	10.0	10.7	14.7
3	2	3	10.0	6.8	13.5
4	3	3	10.0	5.3	14.0
5	2	1	10.0	9.7	20.4
6	2	2	10.0	7.9	14.8

#### 15 Example 6

In this test series, the dewatering and retention effect was evaluated as in Example 3, using a combination of sodium acetate (550 ppm Na<sup>+</sup>) and calcium chloride (1300 ppm Ca<sup>2+</sup>) to adjust the conductivity.

The polymers according to Example 1 were similarly used in this test series. The anionic microparticulate material used was hydrated suspension of powdered Na-bentonite in water. The bentonite had a surface charge of about 0.33 meq/g and a

swelling ability of 41 ml (2 g). The bentonite particles were added in an amount of 8.0 kg/ton, calculated as dry bentonite on dry stock system

Table 6 shows the dewatering and retention effect at various dosages of P1 and P2, calculated as dry polymer on dry stock system.

5

Table 6

Test No.	Polymer Dosage [kg/t]	Bentonite dosage [kg/t]	Conductivity [mS/cm]	Dewatering time [s]		Turbidity [NTU]	
				P1	P2	P1	P2
1	1	8	10.0	13.6	18.5	41	47
2	2	8	10.0	10.8	20.6	29	41
3	3	8	10.0	8.48	24.8	20	36
4	4	8	10.0	7.42	26.6	18	36

Example 7

In this test series, the dewatering effect was evaluated as in Example 6, except that sodium chloride was used to adjust the conductivity.

10

The polymers and bentonite according to Example 6 were similarly used in these tests. The bentonite particles were added in an amount of 8.0 kg/ton, calculated as dry bentonite on dry stock system. Table 7 shows the dewatering and retention effect at various dosages of P1 and P2, calculated as dry polymer on dry stock system.

Table 7

Test No.	Polymer Dosage [kg/t]	Bentonite dosage [kg/t]	Conductivity [mS/cm]	Dewatering time [s]	
				P1	P2
1 2 3 4	2	8	550 ppm Na <sup>+</sup> 2.5	15.3	17.5
	3	8	2.5	11.9	14.1
	4	8	2.5	8.6	9.8
	5	8	2.5	6.8	8.2
5 6 7 8	2	8	3320 ppm Na <sup>+</sup> 10.0	12.7	15.5
	3	8	10.0	9.4	12.5
	4	8	10.0	6.9	10.9
	5	8	10.0	5.6	10.0

15

Example 8

In this test series, the dewatering effect was evaluated as in Example 3, except that zinc chloride was used to adjust the conductivity. The polymers and anionic inorganic particles according to Example 1 were similarly used in these tests.

Table 8 shows the results of the dewatering tests at various dosages of silica-based particles, calculated as  $\text{SiO}_2$  and based on dry stock system.

Table 8

Test No.	Polymer Dosage [kg/t]	$\text{SiO}_2$ dosage [kg/t]	Conductivity [mS/cm]	Dewatering time [s]	
				P1	P2
			700 ppm $\text{Zn}^{2+}$		
1	2	0	2.4	13.6	22.7
2	2	1	2.4	7.9	8.5
3	2	2	2.4	5.5	5.6
			1400 ppm $\text{Zn}^{2+}$		
4	2	0	4.5	18.0	28.0
5	2	2	4.5	6.3	11.4

Claims

1. A process for the production of paper from a suspension containing cellulosic fibres, and optional fillers, comprising adding to the suspension a drainage and retention aid comprising a cationic organic polymer, forming and dewatering the suspension on a wire, characterised in that the cationic organic polymer has an aromatic group and that the suspension which is dewatered on the wire has a conductivity of at least 2.0 mS/cm.

2. A process for the production of paper from a suspension containing cellulosic fibres, and optional fillers, comprising adding to the suspension a drainage and retention aid comprising a cationic organic polymer, forming and dewatering the suspension on a wire to obtain a wet web of paper and white water, characterised in that the cationic organic polymer has an aromatic group and the process further comprising recirculating the white water and optionally introducing fresh water to form a suspension containing cellulosic fibres, and optional fillers, to be dewatered, the amount of fresh water introduced being less than 30 tons per ton of dry paper produced.

3. A process according to claim 1, characterised in that the process further comprises dewatering the suspension on a wire to obtain a wet web of paper and white water, recirculating the white water and optionally introducing fresh water to form a suspension containing cellulosic fibres, and optional fillers, to be dewatered, the amount of fresh water introduced being less than 20 tons per ton of dry paper produced.

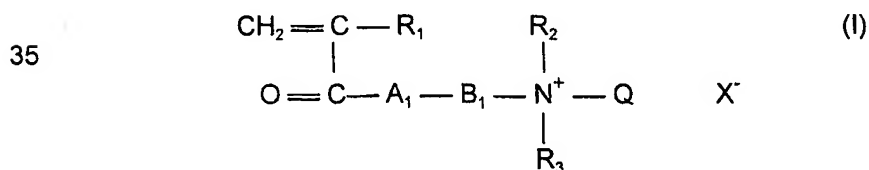
4. A process according to claim 1, 2 or 3, characterised in that the suspension which is dewatered on the wire has a conductivity of at least 5.0 mS/cm.

5. A process according to claim 1, 2, 3 or 4, characterised in that less than 10 tons of fresh water is introduced per ton of dry paper produced.

6. A process according to claim 1, 2, 3, 4 or 5, characterised in that the cationic organic polymer is a vinyl addition polymer comprising in polymerized form one or more monomers comprising at least one monomer having an aromatic group.

7. A process according to any of the preceding claims, characterised in that the cationic organic polymer is an acrylamide-based polymer.

8. A process according to any of the preceding claims, characterised in that the cationic organic polymer comprises in polymerized form a cationic monomer having an aromatic group represented by the general formula (I):



wherein  $R_1$  is H or  $CH_3$ ,  $R_2$  and  $R_3$  are each an alkyl group having from 1 to 3 carbon atoms,  $A_1$  is O or NH,  $B_1$  is an alkylene group of from 2 to 4 carbon atoms or a hydroxy propylene group, Q is benzyl, and  $X^-$  is an anionic counterion.

5           9. A process according to any of the preceding claims, characterised in that the cationic organic polymer has a weight average molecular weight of at least 1,000,000.

10           10. A process according to any of the preceding claims, characterised in that the cationic organic polymer is prepared from a monomer mixture comprising from 5 to 20 mole% of cationic monomer having an aromatic group and from 95 to 80 mole% of other copolymerizable monomers.

11. A process according to any of the preceding claims, characterised in that the drainage and retention aid further comprises anionic inorganic particles.

15           12. A process according to claim 11, characterised in that the anionic inorganic particles are selected from silica-based particles or bentonite.

13. A process according to claim 11 or 12, characterised in that the anionic inorganic particles are selected from aluminium-modified silica-based particles

20           14. A process according to any of the preceding claims, characterised in that the drainage and retention aid further comprises a low molecular weight cationic organic polymer.

15. A process according to any of the preceding claims, characterised in that the drainage and retention aid further comprises an aluminium compound.

25           16. A process according to any of the preceding claims, characterised in that the suspension which is dewatered on the wire has a content of di- and multivalent cations of at least 200 ppm.

17. A process according to any of the preceding claims, characterised in that the suspension comprises recycled fibres.

# INTERNATIONAL SEARCH REPORT

International Application No

PCT/SE 99/00677

## A. CLASSIFICATION OF SUBJECT MATTER

IPC 6 D21H23/08 //D21H21:10, D21H17:20

According to International Patent Classification (IPC) or to both national classification and IPC

## B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC 6 D21H

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

## C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
Y	EP 0 805 234 A (NALCO CHEMICAL CO) 5 November 1997 (1997-11-05) cited in the application page 4, line 27 - line 58 page 7, line 50 - line 54 claims 1,4	1,7-12, 14,16,17
A	the whole document	2-6,13, 15
Y	WO 95 02288 A (PICTURETEL CORP) 19 January 1995 (1995-01-19)  page 7, line 21 - line 34 page 8, line 22 - page 9, line 3 page 12, line 16 - line 26 claim 5	1-3,5,7, 10-12, 14,17
A	the whole document	4,6,8,9, 13,15,16



Further documents are listed in the continuation of box C.



Patent family members are listed in annex.

Special categories of cited documents:

"A" document defining the general state of the art which is not considered to be of particular relevance

"E" earlier document but published on or after the international filing date

"L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)

"O" document referring to an oral disclosure, use, exhibition or other means

"P" document published prior to the international filing date but later than the priority date claimed

"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention

"X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone

"Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.

"Z" document member of the same patent family

Date of the actual completion of the international search

21 July 1999

Date of mailing of the international search report

04/08/1999

Name and mailing address of the ISA

European Patent Office, P.B. 5818 Patentlaan 2  
NL - 2280 HV Rijswijk  
Tel. (+31-70) 340-2040, Tx. 31 651 epo nl,  
Fax: (+31-70) 340-3016

Authorized officer

Naeslund, P

International Application No  
PCT/SE 99/00677

C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT		
Category	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
Y	EP 0 335 575 A (ALLIED COLLOIDS LTD) 4 October 1989 (1989-10-04)  page 3, line 49 - line 55 page 4, line 22 - line 23	1,2,7-9, 11,12, 14,17
A	the whole document  ---	3-6,10, 13,15,16
Y	US 5 098 520 A (BEGALA ARTHUR J) 24 March 1992 (1992-03-24) cited in the application column 5, line 15 - line 25 column 10, line 30 - line 32	1,2,7,9, 11-17
A	the whole document  ---	3-6,8,10
Y	EP 0 752 496 A (EKA CHEMICALS AB) 8 January 1997 (1997-01-08) page 5, paragraph 1	13,15
A	the whole document  & US 5 858 174 A cited in the application  ---	1-12,14, 16,17
Y	A.THORP ET AL: "PULP AND PAPER MANUFACTURE, THIRD EDITION,VOLUME 7, PAPER MACHINE OPERATIONS" 1991, THE JOINT TEXTBOOK COMMITTEE OF THE PAPER INDUSTRY TAPPI/CPPA, ATLANTA,GA,U.S.A. XP002109772 PAGES 598,599	2,3,5
A	  -----	1.4,6-17

# INTERNATIONAL SEARCH REPORT

Information on patent family members

International Application No

PCT/SE 99/00677

Patent document cited in search report		Publication date	Patent family member(s)	Publication date
EP 0805234	A	05-11-1997	AU 1915897 A BR 9701967 A CA 2204050 A NO 972022 A	06-11-1997 15-09-1998 01-11-1997 03-11-1997
WO 9502288	A	19-01-1995	EP 0707763 A JP 9503590 T US 5550924 A	24-04-1996 08-04-1997 27-08-1996
EP 0335575	A	04-10-1989	AT 86693 T AU 3174989 A CA 1322435 A DE 68905208 T ES 2053980 T FI 891465 A, B, JP 2006683 A JP 5029719 B JP 5239800 A KR 9602733 B NO 174724 B US 4913775 A	15-03-1993 28-09-1989 28-09-1993 07-10-1993 01-08-1994 29-09-1989 10-01-1990 06-05-1993 17-09-1993 26-02-1996 14-03-1994 03-04-1990
US 5098520	A	24-03-1992	AT 114178 T AU 656541 B AU 8831991 A DE 69105193 D DE 69105193 T DK 497030 T EP 0497030 A ES 2067155 T FI 913469 A, B. GR 3014980 T JP 2831165 B JP 4245998 A NO 177394 B US 5185062 A	15-12-1994 09-02-1995 30-07-1992 22-12-1994 18-05-1995 18-04-1995 05-08-1992 16-03-1995 26-07-1992 31-05-1995 02-12-1998 02-09-1992 29-05-1995 09-02-1993
EP 0752496	A	08-01-1997	AU 691428 B AU 5830096 A BR 9602943 A CA 2180404 A CN 1145967 A JP 9031885 A NO 962845 A NZ 286923 A PL 315106 A US 5858174 A	14-05-1998 23-01-1997 28-04-1998 08-01-1997 26-03-1997 04-02-1997 08-01-1997 22-09-1997 20-01-1997 12-01-1999